

# Using the ambr® crossflow system, a UF/DF high throughput screening tool, to predict pilot-scale TFF performance during monoclonal antibody processing

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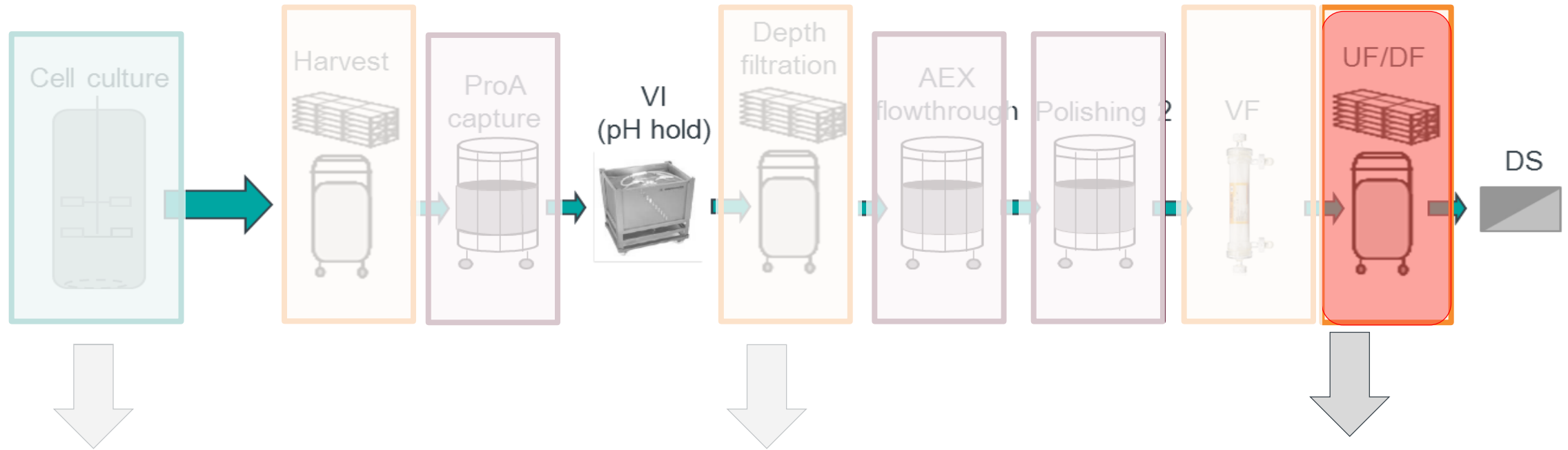
**MSD**

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Session 2: Case studies – Monoclonal antibodies and antibody-like molecules

HTPD Meeting - Porto, Portugal

# High-throughput systems for biologics process development

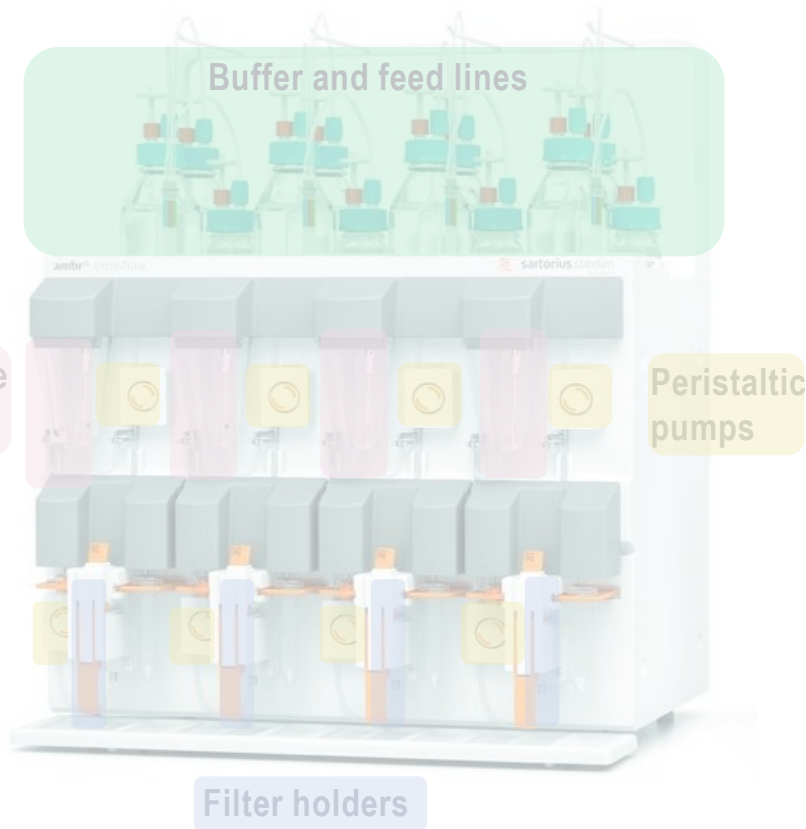


- **High throughput scale-down system:** Ambr® 15 and 250 bioreactors
- **Volume requirements:** 15-250 mL per condition
- **Established in literature** (Manahan et al., 2019; Hsu et al., 2012)

- **High throughput scale-down system:** Robocolumns, 4 or 7 mL columns
- **Volume requirements:** 600  $\mu$ L – 7mL per condition
- **Established in literature** (Evans et al., 2017; Welsh et al., 2014)

- **High throughput scale-down system:** n/a
- **Smallest available format:** Harvest: e.g. 23 cm<sup>2</sup> for A1HC filter  
VF: e.g. 10 cm<sup>2</sup> for Planova  
UF/DF: 88 cm<sup>2</sup> for flat-sheet Pellicon
- **Established in literature (-)**

# Filling the gap with the *ambr*<sup>®</sup> crossflow: a high throughput UF/DF screening tool



### System dimensions per channel

Membrane area (cm <sup>2</sup> )	10
System hold-up volume (mL)	3
Minimum final retentate volume (mL)	5
Typical material requirements per channel (mL)	Protein: 0.1 – 1.0 g (~ 100 – 1000 gm <sup>-2</sup> ) Buffer: ~300 mL (Equilibration, diafiltration & product flush) 0.1 M NaOH: ~150 mL (Filter storage & flush lines)

# Advantages and limitations of the ambr® crossflow system

Advantages	Limitations
<ul style="list-style-type: none"><li>+ Excellent automation</li><li>+ Can run up to 4 conditions at a time (scope up to 16)</li><li>+ Easy data collection</li><li>+ Online data viewing of key parameters (pressures, flux, pH, conductivity, etc)</li><li>+ Flexible recipe method builder</li></ul>	<ul style="list-style-type: none"><li>- The four channels are not totally independent for specific commands</li><li>- Limited filter choice:<ul style="list-style-type: none"><li>• Screen: custom-made (no choice of screen)</li><li>• Composition: Only regenerated cellulose</li><li>• Pore size: 10 and 30 kDa</li></ul></li><li>- Designed for formulation applications using high viscosity solutions<ul style="list-style-type: none"><li>• Typical incoming concentration for UF/DF ~ 2 – 10 g/L which has a water-like viscosity characteristic</li></ul></li></ul>

# Part 1: Proof-of-concept screening experiments with ambr<sup>®</sup> crossflow

# Screening studies:

*using the ambr<sup>®</sup> crossflow to identify molecule-specific behavior early on*

## Input screened Parameters:

- Transmembrane pressure
- Loading
- Diafiltration concentration
- Feed composition

## Output metrics:

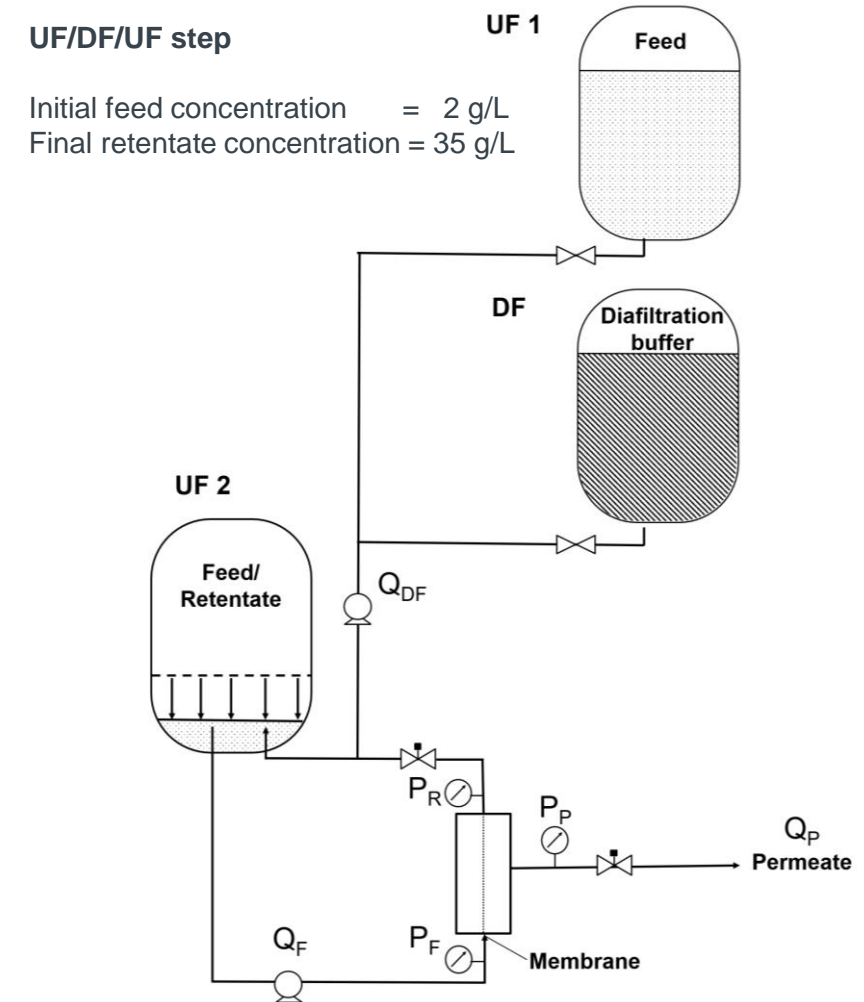
- Membrane performance (permeate flux, J)
- Product quality (Change in high molecular weight,  $\Delta$ HMW by UP-SEC)

# number of UF/DF/UF runs: 11

Total protein required: 3.2 g

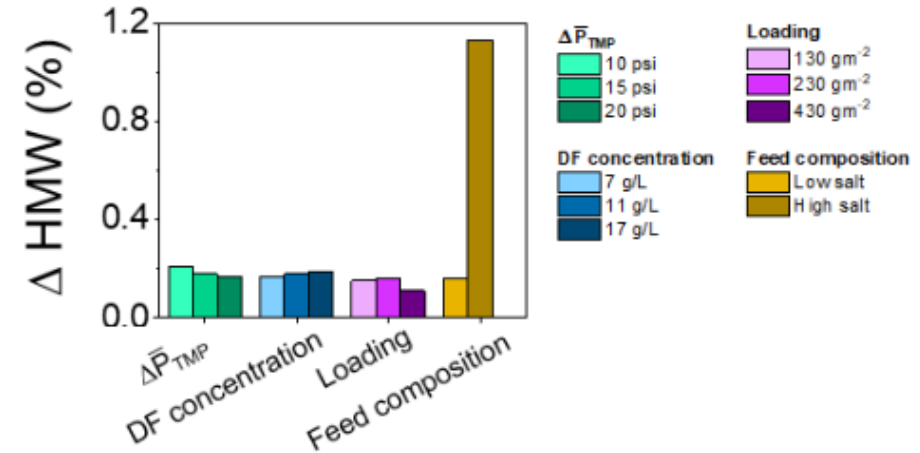
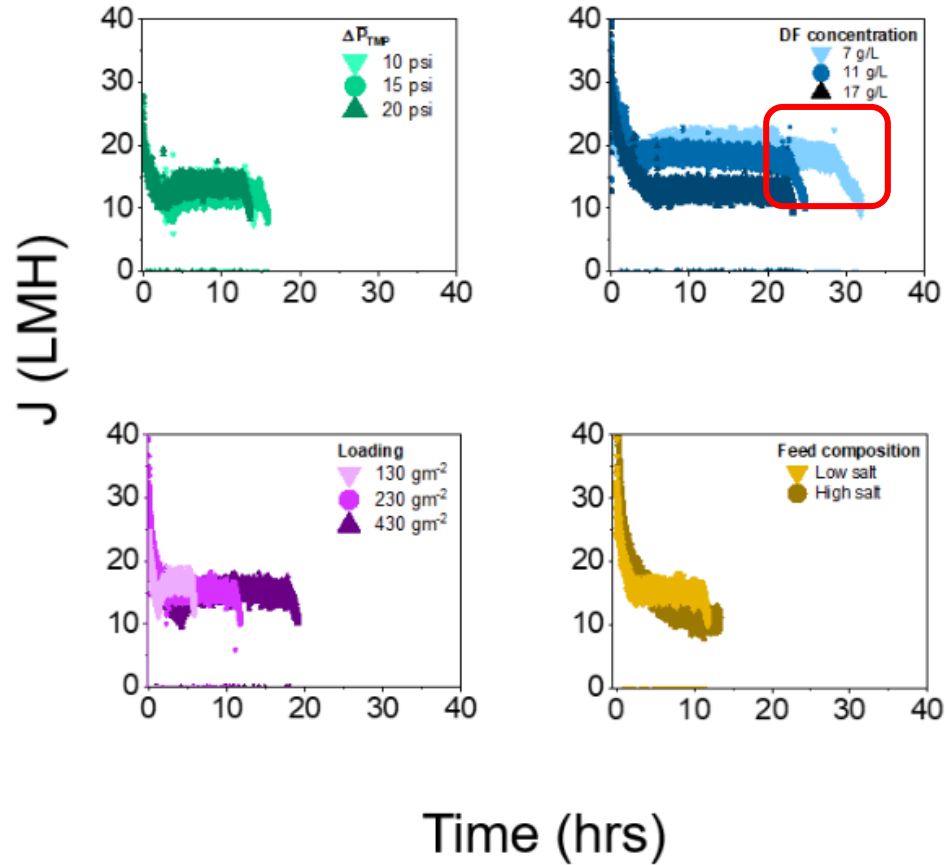
Total buffer needed: ~1.3 L

Total resources required: ~ 40 hrs



# Screening studies:

*This data can help inform early on process development decisions*



- Only loading and DF concentration > 11 g/L significantly impact permeate flux (J)
- Only feed composition affects product quality (%  $\Delta HMW$ )

# Part 2: How scalable is the ambr® crossflow data?



# Scale translation with traditional TFF system

**Method:** Compare performance between ambr® crossflow and qualified TFF system

**Conditions** Loading : 230 g of protein per m<sup>2</sup> of membrane area

Q<sub>F</sub> : 7 LMM

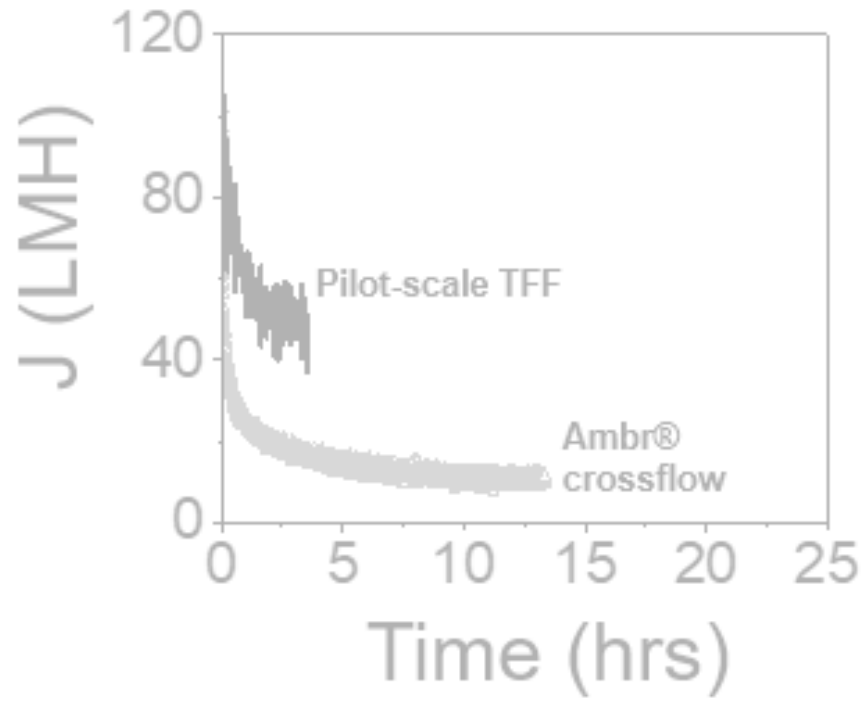
ΔP<sub>TMP</sub> : 15 psi

2 g/L (initial) → 25 g/L (diafiltration) → 35 g/L (final) concentration

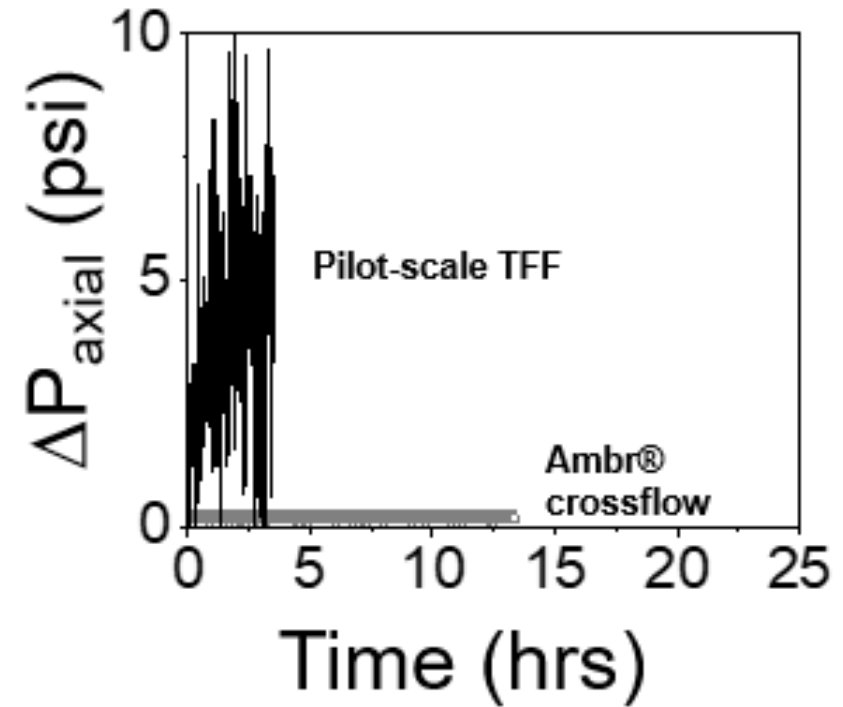
	TFF	Ambr® crossflow
Area (cm <sup>2</sup> )	176 cm <sup>2</sup> (2 x 88cm <sup>2</sup> )	10 cm <sup>2</sup>
Type of pump (-)	Quaternary Diaphragm Quattroflow™	Peristaltic ambr®-proprietary
System hold-up volume (mL)	50	3
Volume required per run (mL)	2500	140
Volumetric loading (L/m <sup>2</sup> )		142
Scale-down ratio (-)		1:18

# Scale comparison:

*There is a mismatch between scales*



- Ambr® crossflow data underpredicts flux by 3-fold ( $t_{\text{total}} = 14$  vs. 4 hrs)



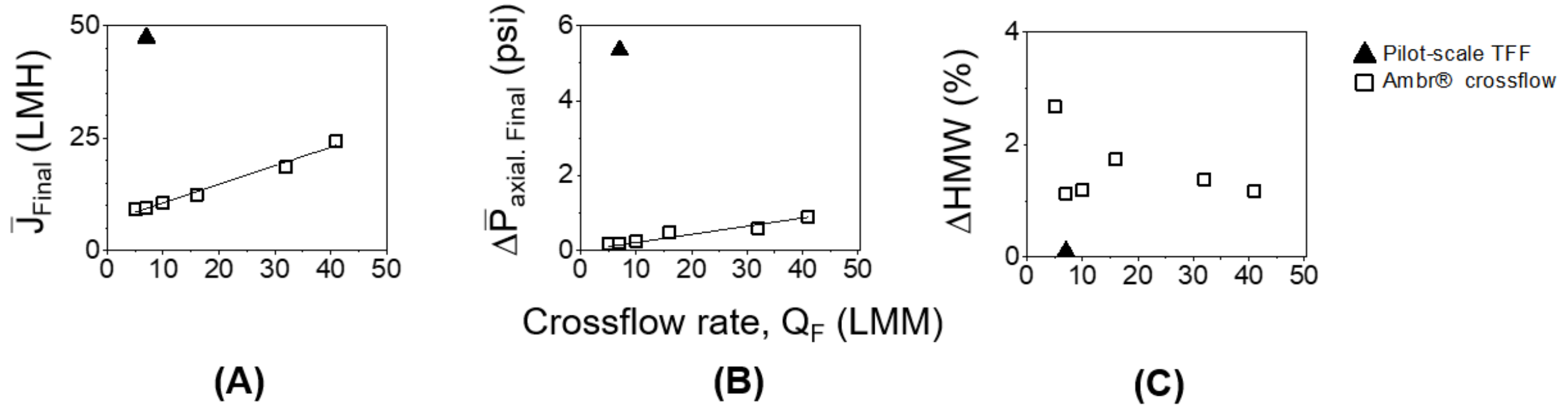
- Axial pressure drop,  $\Delta P_{\text{axial}}$  ( $P_{\text{feed}} - P_{\text{retentate}}$ ) does not match either.
  - ✓ It is not a typical scale-down parameter, but it should be within a similar range to obtain comparable membrane performance

230  $\text{gm}^{-2}$ ,  $Q_F = 7$  LMM,  $\Delta P_{\text{TMP}} = 15$  psi  
Initial feed concentration = 2 g/L  
Diafiltration concentration = 25 g/L  
Final retentate concentration = 35 g/L

# Part 3: Evaluating different strategies to improve the match between scales

# Strategy I:

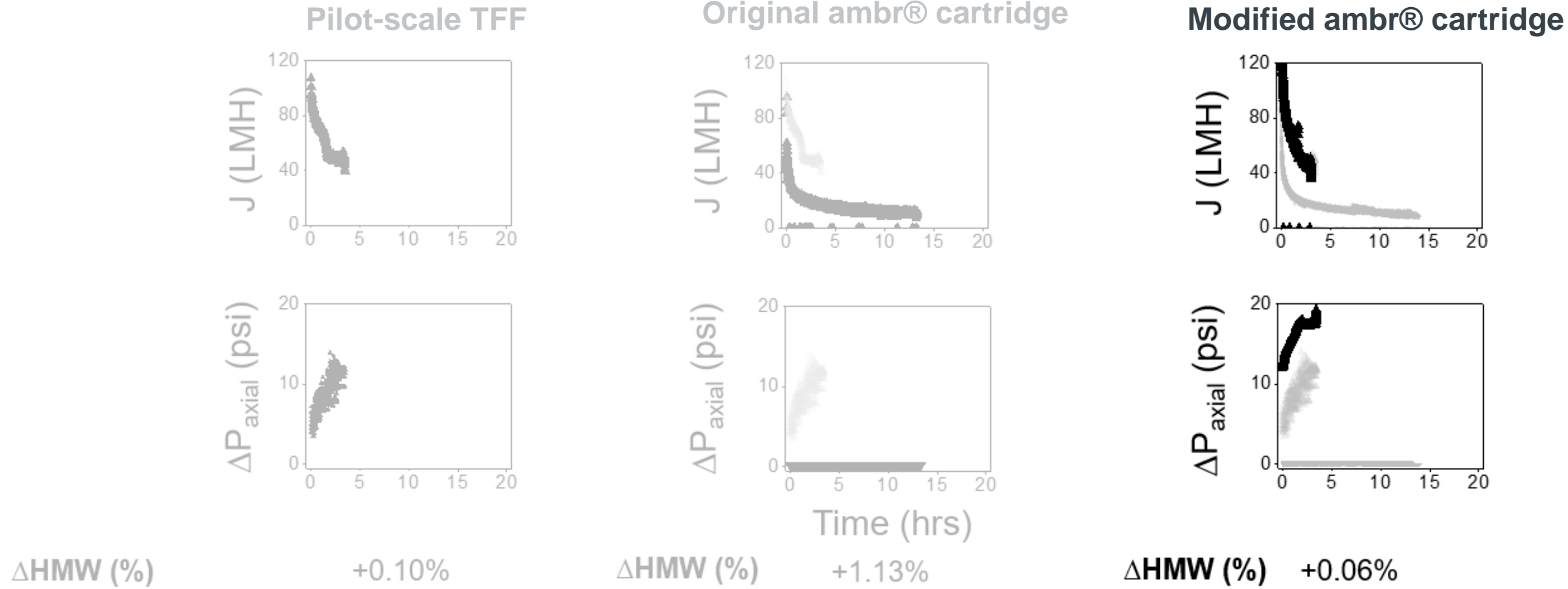
Increase crossflow rate in the ambr® crossflow



- Expected behavior of ambr® crossflow with increasing crossflow rate (5 - 42 LMM)
- However, no progress in match between systems even with the 42 LMM ambr® crossflow run

# Strategy 2:

Modify the ambr® cartridge to reproduce flat-sheet behavior



- Significant improvement between original ambr® and modified ambr® cartridge
- Match in flux and product quality, and similar range  $\Delta P_{axial}$

# Part 4: Testing the modified ambr® cartridge across a typical DoE space

# Comparing ambr® crossflow with qualified TFF system

**Method:** Compare performance between ambr® crossflow and our qualified TFF system

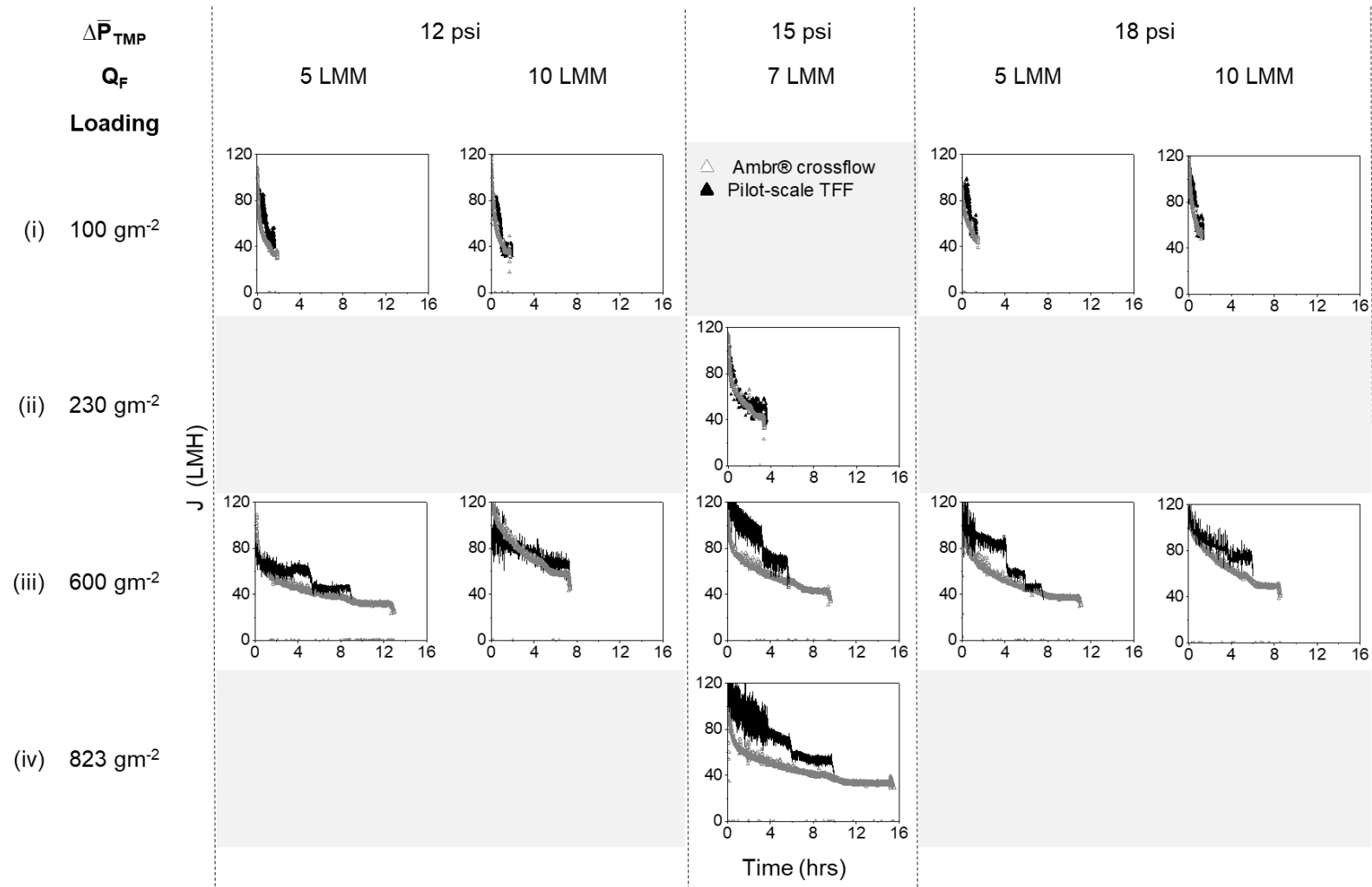
**Conditions:** Using  $2^3$  full factorial central composite design (CCD) design of experiments (DoE)

Loading: 100 – 230 – 600  $\text{gm}^{-2}$  (+ 823  $\text{gm}^{-2}$ )

$\Delta P_{\text{TMP}}$  : 12 – 15 – 18 psi

Crossflow rate: 5 – 7 – 10 LMM

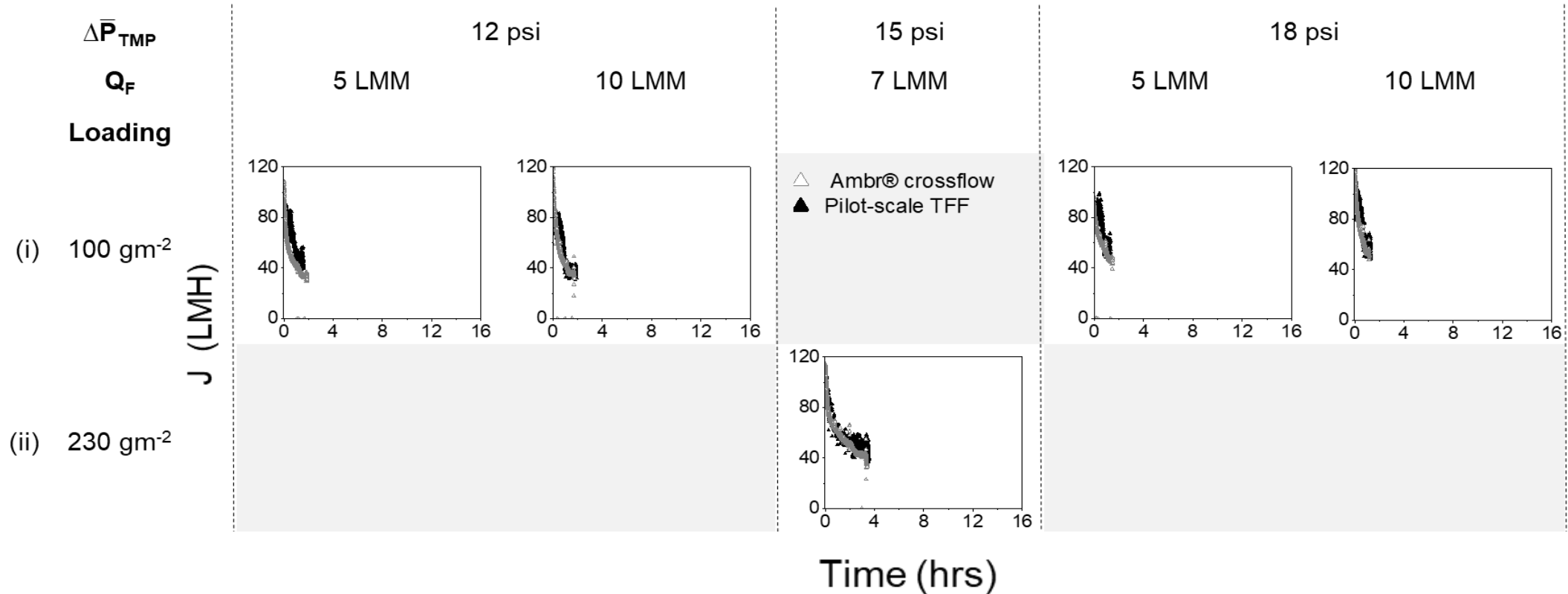
# Comparing performance across scales: Good agreement across the DoE conditions tested



- Increased overall comparability with modified ambr® cartridge runs

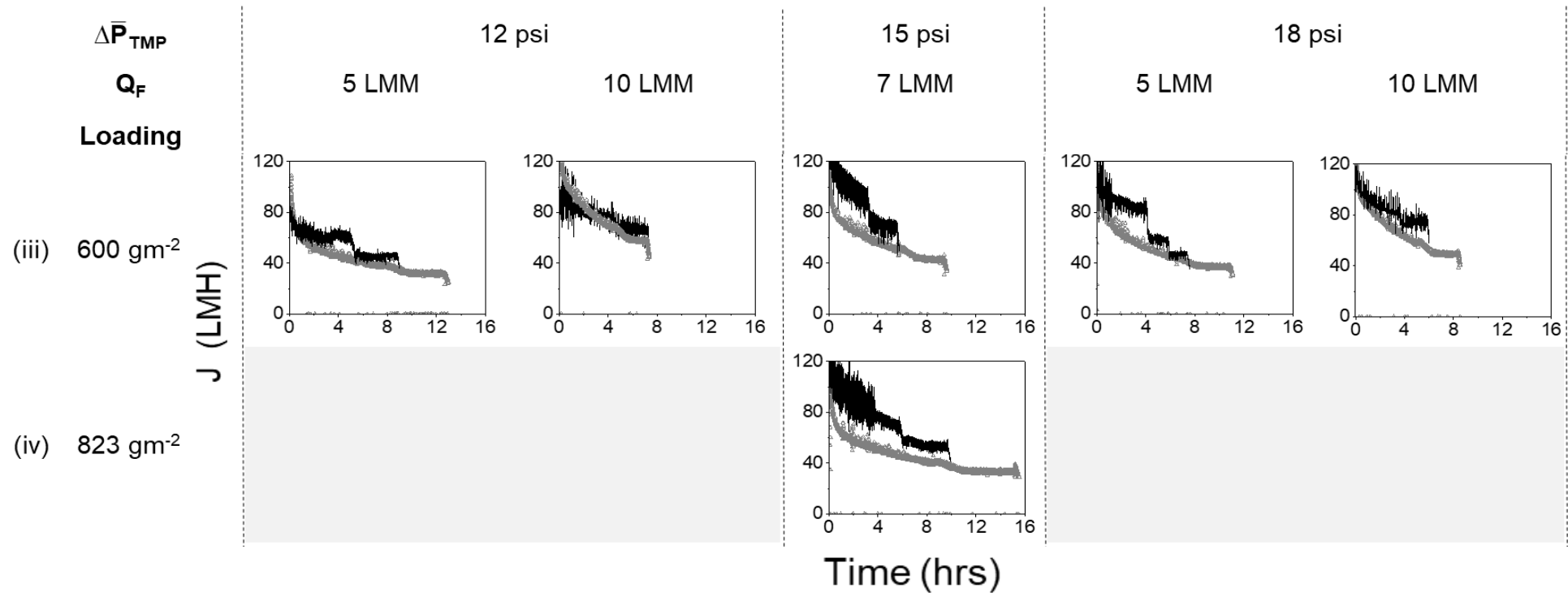


# Comparing performance across scales: Flux matches well at low loadings



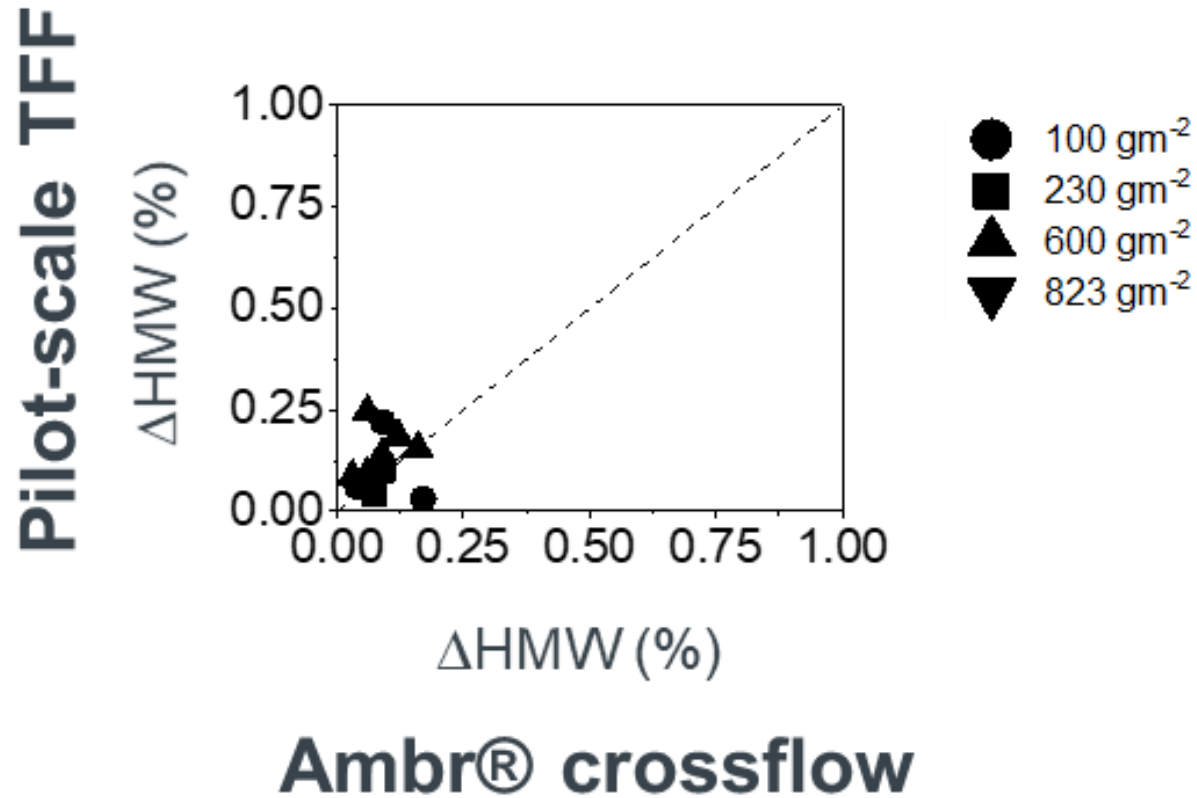
- Good agreement at 100 and  $230 \text{ gm}^{-2}$  conditions. At both scales:
  - ✓  $100 \text{ gm}^{-2}$  runs take < 2 hrs
  - ✓  $230 \text{ gm}^{-2}$  take ~4 hrs

# Comparing performance across scales: Flux starts deviating at higher loadings



- Disparity in flux starts to appear at higher loadings.
- Possible differences that could explain this:
  - ✓ Membrane path length across scales
  - ✓ System set-up (i.e. pump type, system hold-up volume, shear rate)

# Comparing performance across scales: Product quality is similar across DoE in both scales



- All conditions at both scales result in < 0.25%  $\Delta$ HMW (%) during UF/DF/UF step

# Way forward

# Summary

## 1. Proof-of-concept screening ambr® crossflow studies

- Only a fraction of resources needed



## 2. Side-by-side comparison with a qualified TFF system

- Differences in the membrane performance were attributed to the ambr® cartridge configuration.



## 3. Modification of the ambr® cartridge

- With a view to better reproduce the flat-sheet cassette performance



## 4. Comparable product quality and fluxes across DoE study at both scales

- Better agreement found at low loadings

# What's next?

- Work towards establishing ambr® crossflow system as a process characterization tool by:
  - ✓ Qualify as scale-down model by investigating key outputs – HMW (%), flux, and/or yield?
  - ✓ Evaluating additional mAb molecules
- Work with vendor to develop manufacturing capabilities of different ambr® cartridges to suit a wider range of bioprocessing applications

# Acknowledgements

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THANK YOU.  
QUESTIONS?